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AMENDMENT TO THE CLAIMS

This listing of claims will replace all prior versions and listings of claims in the application.

Listing of Claims

1. (Originally Presented) A process of reducing NO_x emissions from the regeneration zone during fluid catalytic cracking of a hydrocarbon feedstock into lower molecular weight components, said process comprising
 - a) contacting a hydrocarbon feedstock during a fluid catalytic cracking (FCC) process wherein NO_x emissions are released from a regeneration zone of a fluid catalytic cracking unit (FCCU) operating under FCC conditions with a circulating inventory of an FCC cracking catalyst and a particulate NO_x reduction catalyst/additive composition having a mean particle size of greater than 45 μm and comprising (i) at least 10 weight percent of a NO_x reduction zeolite component selected from the group consisting of ZSM-11, beta, MCM-49, mordenite, MCM-56, Zeolite-L, zeolite Rho, errionite, chabazite, clinoptilolite, MCM-22, MCM-35, MCM-61, Offretite, A, ZSM-12, ZSM-23, ZSM-18, ZSM-22, ZSM-57, ZSM-61, ZK-5, NaJ, Nu-87, Cit-1, SSZ-35, SSZ-48, SSZ-44, SSZ-23, Dachiardite, Merlinoite, Lovdarite, Levyne, Laumontite, Epistilbite, Gmelonite, Gismondine, Cancrinite, Brewsterite, Stilbite, Paulingite, Goosecreekite, Natrolite, omega or mixtures thereof, and (ii) from about 5 to about 50 weight percent of an inorganic binder selected from the group consisting of alumina, silica, silica alumina, alumina phosphate and mixtures thereof; and
 - b) reducing the amount of NO_x emissions released from the regeneration zone of the FCCU by at least 10% as compared to the amount of NO_x emissions released in the absence of the particulate NO_x reduction composition.
2. (Originally Presented) The process of Claim 1 wherein the FCC cracking catalyst comprises a Y-type zeolite.

3. (Currently Amended) The process of Claim 1 wherein step (b) is accomplished without a substantial ~~reduction~~ change in the hydrocarbon feedstock conversion or yield of cracked hydrocarbons as compared to the hydrocarbon feedstock conversion or yield of cracked hydrocarbons obtained from the cracking catalyst alone.
4. (Currently Amended) The process of Claim ~~3~~ 1 wherein the amount of the NO_x reduction zeolite component present in the catalyst/additive composition is at least 30 weight percent of the composition.
5. (Originally Presented) The process of Claim 4 wherein the amount of the NO_x reduction zeolite component present in the catalyst/additive composition is at least 40 weight percent of the composition.
6. (Originally Presented) The process of Claim 5 wherein the amount of the NO_x reduction zeolite component present in the catalyst/additive composition is at least 50 weight percent of the composition.
7. (Currently Amended) The process of Claim ~~3~~ 1 wherein the amount of the NO_x reduction zeolite component present in the catalyst/additive composition ranges from about 10 to about 85 weight percent of the composition.
8. (Originally Presented) The process of Claim 7 wherein the amount of the NO_x reduction zeolite component present in the catalyst/additive composition ranges from about 30 to about 80 weight percent of the composition.
9. (Originally Presented) The process of Claim 8 wherein the amount of the NO_x reduction zeolite component present in the catalyst/additive composition ranges from about 40 to about 75 weight percent of the composition.

10. (Currently Amended) The process of Claim 1 or 3 wherein the NO_x reduction zeolite component is exchanged with a cation selected from the group consisting of hydrogen, ammonium, alkali metal and combinations thereof.
11. (Currently Amended) The process of Claim 3_1 wherein the NO_x reduction zeolite component further comprises at least one stabilizing metal.
12. (Originally Presented) The process of Claim 11 wherein the stabilizing metal is a metal selected from the group consisting of Groups 2A, 3B, 4B, 5B, 6B, 7B, 8B, 2B, 3A, 4A, 5A, and the Lanthanide Series of The Periodic Table, Ag and mixtures thereof.
13. (Originally Presented) The process of Claim 12 wherein the stabilizing metal is selected from the group consisting of Groups 3B, 2A, 2B, 3A and the Lanthanide Series of the Periodic Table, and mixtures thereof.
14. (Originally Presented) The process of Claim 13 wherein the stabilizing metal is selected from the group consisting of lanthanum, aluminum, magnesium and zinc, and mixtures thereof.
15. (Currently Amended) The process of Claims 11 wherein the stabilizing metal is incorporated into the pores of the NO_x reduction zeolite component.
16. (Originally Presented) The process of Claim 1 wherein the inorganic binder is selected from the group consisting of silica, alumina, silica alumina and mixtures thereof.
17. (Originally Presented) The process of Claim 16 wherein the inorganic binder is alumina.

18. (Originally Presented) The process of Claim 17 wherein the alumina is an acid or base peptized alumina.
19. (Originally Presented) The process of Claim 17 wherein the alumina is aluminum chlorohydrol.
20. (Currently Amended) The process of Claim ~~3~~1 wherein the amount of inorganic binder present in the particulate catalyst/additive composition ranges from about 10 to about 30 weight percent of the composition.
21. (Originally Presented) The process of Claim 20 wherein the amount of inorganic binder present in the particulate catalyst/additive composition ranges from about 15 to about 25 weight percent of the composition.
22. (Originally Presented) The process of Claim 1 wherein the NO_x reduction zeolite component has a SiO₂ to Al₂O₃ molar ratio of less than 500.
23. (Originally Presented) The process of Claim 1 wherein the NO_x reduction zeolite component is a zeolite selected from the group consisting of beta, MCM-49, mordenite, MCM-56, Zeolite-L, zeolite Rho, errionite, chabazite, clinoptilolite, MCM-22, Offretite, A, ZSM-12, ZSM-23, omega and mixtures thereof.
24. (Currently Amended) The process of Claim ~~3~~1 wherein the particulate catalyst/additive composition further comprises an additional zeolite other than the NO_x reduction zeolite.
25. (Originally Presented) The process of claim 24 wherein the additional zeolite is selected from the group consisting of ferrierite, ZSM-5, ZSM-35 and mixtures thereof.

26. (Originally Presented) The process of Claim 24 or 25 wherein the additional zeolite is present in an amount ranging from about 1 to about 80 weight percent of the composition.
27. (Originally Presented) The process of Claim 26 wherein the additional zeolite is present in an amount ranging from about 10 to about 70 weight percent of the composition.
28. (Originally Presented) The process of Claim 1 or 3 wherein the catalyst/additive composition further comprises a matrix material selected from the group consisting of alumina, silica, silica alumina, titania, zirconia, yttria, lanthana, ceria, neodymia, samaria, europia, gadolinia, praseodymia, and mixtures thereof.
29. (Originally Presented) The process of Claim 28 wherein the matrix material is present in an amount less than 70 weight percent.
30. (Currently Amended) The process of Claim 1 or 3 further comprising recovering the cracking catalyst from said contacting step and treating the used catalyst in a regeneration zone to regenerate said catalyst.
31. (Originally Presented) The process of Claim 30 wherein the cracking catalyst and the particulate catalyst/additive composition are fluidized during contacting said hydrocarbon feedstock.
32. (Currently Amended) The process of Claim 1 or 3 further comprising contacting the hydrocarbon feed with at least one additional NO_x reduction composition.
33. (Originally Presented) The process of Claim 32 wherein the additional NO_x reduction composition is a non-zeolitic composition.

34. (Originally Presented) The process of Claim 33 wherein the additional NO_x reduction composition comprises (1) an acidic metal oxide containing substantially no zeolite; (2) a metal component, measured as the oxide, selected from the group consisting of an alkali metal, an alkaline earth metal and mixtures thereof; (3) an oxygen storage metal oxide component; and (4) at least one noble metal component.
35. (Currently Amended) The process of Claim 32 wherein the additional NO_x reduction composition is a low NO_x, CO combustion promoter composition which comprises (1) an acidic oxide support; (2) an alkali metal and/or alkaline earth metal or mixtures thereof; (3) a transition metal oxide having oxygen storage capability; and (4) palladium.
36. (Originally Presented) The process of Claim 32 wherein the additional NO_x reduction composition comprises (1) an acidic oxide support; (2) an alkali metal and/or alkaline earth metal or mixtures thereof; (3) a transition metal oxide having oxygen storage capability; and (4) a transition metal selected from Groups IB and IIB of the Periodic Table, and mixtures thereof.
37. (Originally Presented) The process of Claim 32 wherein the additional NO_x reduction composition comprises at least one metal-containing spinel which includes a first metal and a second metal having a valence higher than the valence of said first metal, at least one component of a third metal other than said first and second metals and at least one component of a fourth metal other than said first, second and third metals, wherein said third metal is selected from the group consisting of Group IB metals, Group IIB metals, Group VIA metals, the rare-earth metals, the Platinum Group metals and mixtures thereof, and said fourth metal is selected from the group consisting of iron, nickel, titanium, chromium, manganese, cobalt, germanium, tin, bismuth, molybdenum, antimony, vanadium and mixtures thereof.

38. (Originally Presented) The process of Claim 37 wherein the metal containing spinel comprises magnesium as said first metal and aluminum as said second metal.
39. (Originally Presented) The process of Claim 38 wherein the third metal component in the metal containing spinel is selected from the group consisting of a Platinum Group metal, the rare-earth metals and mixtures thereof.
40. (Originally Presented) The process of Claim 39 wherein the third metal component is present in an amount in the range of about 0.001 to about 20 weight percent, calculated as elemental third metal.
41. (Originally Presented) The process of Claim 40 wherein said fourth metal component is present in an amount in the range of about 0.001 to about 10 weight percent, calculated as elemental fourth metal.
42. (Originally Presented) The process of Claim 32 wherein the additional NO_x reduction additive is a zinc based catalyst.
43. (Originally Presented) The process of Claim 32 wherein the additional NO_x reduction additive is an antimony based NO_x reduction additive.
44. (Originally Presented) The process of Claim 32 wherein the additional NO_x reduction additive is a pervoskite-spinel NO_x reduction additive.
45. (Originally Presented) The process of Claim 32 wherein the additional NO_x reduction additive is a hydrotalcite containing composition.
46. (Originally Presented) The process of Claim 32 wherein the additional NO_x reduction composition comprises (i) an acidic metal oxide, (ii) cerium oxide, (iii) a lanthanide oxide other than ceria, and (iv) optionally, at least

one oxide of a transition metal selected from Groups IB and IIB of the Periodic Table, and mixtures thereof.

47. (Currently Amended) The process of Claim ~~3~~1 wherein the particulate NO_x reduction composition has a mean particle size from about 50 to about 200 μm.
48. (Originally Presented) The process of Claim 47 wherein the particulate NO_x reduction composition has a mean particle size from about 55 to about 150 μm.
49. (Currently Amended) The process of Claim 1 or ~~2~~3 wherein the particulate NO_x reduction composition has a Davison attrition index (DI) value of less than 50.
50. (Originally Presented) The process of Claim 49 wherein the particulate NO_x reduction composition has a DI value of less than 20.
51. (Originally Presented) The process of Claim 50 wherein the particulate NO_x reduction composition has a DI value of less than 15.
52. (Originally Presented) The process of Claim 2 wherein the amount of the catalyst/additive composition in the catalyst inventory is that amount sufficient to provide a ratio of NO_x reduction zeolite component to Y-type zeolite in the total catalyst inventory of less than 2.
53. (Originally Presented) The process of Claim 52 wherein the ratio of NO_x reduction zeolite component to Y-type zeolite in the total catalyst inventory is less than 1.
54. (Originally Presented) The process of Claim 2 wherein step (b) is accomplished without a substantial change in the hydrocarbon feedstock conversion or yield of cracked hydrocarbons as compared to the

hydrocarbon feedstock conversion or yield of cracked hydrocarbons obtained from the cracking catalyst alone.

55. (Originally Presented) A fluid cracking catalyst (FCC) composition, which composition comprises (a) a FCC cracking component suitable for catalyzing the cracking of hydrocarbons under FCC conditions, and (b) a particulate NO_x reduction catalyst/additive composition having a mean particle size of greater than 45 μm and comprising (i) at least 10 weight percent of NO_x reduction zeolite component selected from the group consisting of ZSM-11, beta, MCM-49, mordenite, MCM-56, Zeolite-L, zeolite Rho, errionite, chabazite, clinoptilolite, MCM-22, MCM-35, MCM-61, Offretite, A, ZSM-12, ZSM-23, ZSM-18, ZSM-22, ZSM-57, ZSM-61, ZK-5, NaJ, Nu-87, Cit-1, SSZ-35, SSZ-48, SSZ-44, SSZ-23, Dachiardite, Merlinoite, Lovdarite, Levyne, Laumontite, Epistilbite, Gmelonite, Gismondine, Cancrinite, Brewsterite, Stilbite, Paulingite, Goosecreekite, Natrolite, omega or mixtures thereof, and (ii) about 5 to about 50 weight percent of an inorganic binder selected from the group consisting of alumina, silica, silica alumina, alumina phosphate, and mixtures thereof.
56. (Originally Presented) The catalyst of Claim 55 wherein the FCC cracking component contains a Y-type zeolite.
57. (Originally Presented) The catalyst of Claim 56 wherein the catalyst/additive composition is present in the total catalyst inventory in an amount sufficient to provide a ratio of NO_x reduction zeolite component to Y-type zeolite of less than 2.
58. (Originally Presented) The catalyst of Claim 55 wherein the amount of NO_x reduction zeolite component present in the catalyst/additive composition is at least 30 weight percent of the composition.

59. (Originally Presented) The catalyst of Claim 58 wherein the amount of NO_x reduction zeolite component present in the catalyst/additive composition is at least 40 weight percent of the composition.
60. (Originally Presented) The catalyst of Claim 59 wherein the amount of NO_x reduction zeolite component present in the catalyst/additive composition is at least 50 weight percent of the composition.
61. (Originally Presented) The catalyst of Claim 55 wherein the amount of NO_x reduction zeolite component present in the catalyst/additive composition ranges from about 10 to about 85 weight percent of the composition.
62. (Originally Presented) The catalyst of Claim 61 wherein the amount of NO_x reduction zeolite component present in the catalyst/additive composition ranges from about 30 to about 80 weight percent of the composition.
63. (Originally Presented) The catalyst of Claim 62 wherein the amount of NO_x reduction zeolite component present in the catalyst/additive composition ranges from about 40 to about 75 weight percent of the composition.
64. (Originally Presented) The catalyst of Claim 55 wherein the NO_x reduction zeolite component is exchanged with a cation selected from the group consisting of hydrogen, ammonium, alkali metal and combinations thereof.
65. (Originally Presented) The catalyst of Claim 55 wherein the NO_x reduction zeolite component further comprises at least one stabilizing metal.

66. (Originally Presented) The catalyst of Claim 65 wherein the stabilizing metal is a metal selected from the group consisting of Groups 2A, 3B, 4B, 5B, 6B, 7B, 8B, 2B, 3A, 4A, 5A and the Lanthanide Series of The Periodic Table, Ag and mixtures thereof.
67. (Originally Presented) The catalyst of Claim 66 wherein the stabilizing metal is selected from the group consisting of Groups 3B, 2A, 2B, 3A and the Lanthanide Series of the Periodic Table, and mixtures thereof.
68. (Originally Presented) The catalyst of Claim 67 wherein the stabilizing metal is selected from the group consisting of lanthanum, aluminum, magnesium and zinc, and mixtures thereof.
69. (Originally Presented) The catalyst of Claim 65 wherein the stabilizing metal is incorporated into the pores of the NO_x reduction zeolite component.
70. (Originally Presented) The catalyst of Claim 55 wherein the inorganic binder in the particulate catalyst/additive composition is selected from the group consisting of silica, alumina, silica alumina and mixtures thereof.
71. (Originally Presented) The catalyst of Claim 70 wherein the inorganic binder is alumina.
72. (Originally Presented) The catalyst of Claim 71 wherein the inorganic binder is an aluminum chlorohydrol.
73. (Originally Presented) The catalyst of Claim 71 wherein the alumina is an acid or base peptized alumina.
74. (Originally Presented) The catalyst of Claim 55 wherein the amount of inorganic binder present in the particulate catalyst/additive composition ranges from about 10 to about 30 weight percent of the composition.

75. (Originally Presented) The catalyst of Claim 74 wherein the amount of inorganic binder present in the particulate catalyst/additive composition ranges from about 15 to about 25 weight percent of the composition.
76. (Originally Presented) The catalyst of Claim 55 wherein the NO_x reduction zeolite component is selected from the group consisting of beta, MCM-49, mordenite, MCM-56, Zeolite-L, zeolite Rho, erionite, chabazite, clinoptilolite, MCM-22, Offretite, A, ZSM-12, ZSM-23, omega and mixtures thereof.
77. (Originally Presented) The catalyst of Claim 55 wherein the NO_x reduction zeolite component has a SiO₂ to Al₂O₃ molar ratio of less than 500.
78. (Originally Presented) The catalyst of Claim 55 wherein the particulate catalyst/additive composition further comprises a zeolite other than the NO_x reduction zeolite component.
79. (Currently Amended) The catalyst of Claim 78 wherein the other zeolite is a zeolite selected from the group ~~selected from~~ consisting of ferrierite, ZSM-5, ZSM-35 and mixtures thereof. |
80. (Originally Presented) The catalyst of Claim 78 wherein the other zeolite is present in an amount ranging from about 1 to about 80 weight percent of the composition.
81. (Originally Presented) The catalyst of Claim 80 wherein the other zeolite is present in an amount ranging from about 10 to about 70 weight percent of the composition.
82. (Originally Presented) The catalyst of Claim 55 wherein the composition further comprises a matrix material selected from the group consisting of

alumina, silica, silica alumina, titania, zirconia, yttria, lanthana, ceria, neodymia, samaria, europia, gadolinia, praseodymia and mixtures thereof.

83. (Originally Presented) The catalyst of Claim 82 wherein the matrix material is present in an amount less than 70 weight percent.
84. (Originally Presented) The catalyst of Claim 55 further comprising at least one additional NO_x reduction composition.
85. (Originally Presented) The catalyst of Claim 84 wherein the additional NO_x reduction composition is a non-zeolitic composition.
86. (Originally Presented) The catalyst of Claim 85 wherein the additional NO_x reduction composition comprises (a) an acidic metal oxide containing substantially no zeolite; (b) a metal component, measured as the oxide, selected from the group consisting of an alkali metal, an alkaline earth metal and mixtures thereof; (c) an oxygen storage metal oxide component; and, (d) at least one noble metal component.
87. (Originally Presented) The catalyst of Claim 84 wherein the additional NO_x reduction composition comprises (a) an acidic metal oxide support; (b) an alkali metal, alkaline earth metal or mixtures thereof; (c) a transition metal oxide having oxygen storage capability; and, (d) a transition metal selected from Groups IB and IIB of the Periodic Table, and mixtures thereof.
88. (Currently Amended) The catalyst of Claim 84 wherein the additional NO_x reduction composition is a low NO_x CO combustion promoter composition which comprises (a) an acidic oxide support; (b) an alkali metal, an alkaline earth metal or mixtures thereof; (c) a transition metal oxide having oxygen storage capability; and (d) palladium.

89. (Originally Presented) The catalyst of Claim 84 wherein the additional NO_x reduction composition comprises at least one metal-containing spinel which includes a first metal and a second metal having a valence higher than the valence of said first metal, at least one component of a third metal other than said first and second metals and at least one component of a fourth metal other than said first, second and third metals, wherein said third metal is selected from the group consisting of Group IB metals, Group IIB metals, Group VIA metals, the rare-earth metals, the Platinum Group metals and mixtures thereof, and said fourth metal is selected from the group consisting of iron, nickel, titanium, chromium, manganese, cobalt, germanium, tin, bismuth, molybdenum, antimony, vanadium and mixtures thereof.
90. (Originally Presented) The catalyst of Claim 89 wherein the metal containing spinel comprises magnesium as said first metal and aluminum as said second metal.
91. (Originally Presented) The catalyst of Claim 89 wherein the third metal component in the metal containing spinel is selected from the group consisting of a Platinum Group metal, the rare-earth metals and mixtures thereof.
92. (Originally Presented) The catalyst of Claim 89 wherein the third metal component is present in an amount in the range of about 0.001 to about 20 weight percent, calculated as elemental third metal.
93. (Originally Presented) The catalyst of Claim 89 wherein said fourth metal component is present in an amount in the range of about 0.001 to about 10 weight percent, calculated as elemental fourth metal.
94. (Originally Presented) The catalyst of Claim 84 wherein the additional NO_x reduction additive is a zinc based catalyst.

95. (Originally Presented) The catalyst of Claim 84 wherein the additional NO_x reduction additive is an antimony based NO_x reduction additive.
96. (Originally Presented) The catalyst of Claim 84 wherein the additional NO_x reduction additive is a pervoskite-spinel NO_x reduction additive.
97. (Originally Presented) The catalyst of Claim 84 wherein the additional NO_x reduction additive is a hydrotalcite containing composition.
98. (Originally Presented) The catalyst of Claim 55 wherein the particulate catalyst/additive composition has a mean particle size from about 50 to about 200 μm.
99. (Originally Presented) The catalyst of Claim 98 wherein the particulate catalyst/additive composition has a mean particle size from about 55 to about 150 μm.
100. (Originally Presented) The catalyst of Claim 55 wherein the particulate catalyst/additive composition has a Davison attrition index (DI) value of less than 50.
101. (Originally Presented) The catalyst of Claim 100 wherein the particulate catalyst/additive composition has a DI value of less than 20.
102. (Originally Presented) The catalyst of Claim 101 wherein the particulate catalyst/additive composition has a DI value of less than 15.
103. (Originally Presented) The catalyst of Claim 84 wherein the additional NO_x reduction composition comprises (i) an acidic metal oxide, (ii) cerium oxide, (iii) a lanthanide oxide other than ceria, and (iv) optionally, at least one oxide of a transition metal selected from Groups IB and IIB of the Periodic Table, and mixtures thereof.

104. (Originally Presented) The catalyst of Claim 55 wherein the ratio of NO_x reduction zeolite component to Y-type zeolite in the total catalyst inventory is less than 1.
105. (Originally Presented) A method of reducing NO_x emissions from the regeneration zone during fluid catalytic cracking of a hydrocarbon feedstock into lower molecular weight components, said method comprising contacting a hydrocarbon feedstock with a cracking catalyst at elevated temperature whereby lower molecular weight hydrocarbon components are formed, said cracking catalyst comprising the composition of Claim 55, 56, 57 or 84.
106. (Originally Presented) The method of Claim 105 further comprising recovering the cracking catalyst from said contacting step and treating the used catalyst in a regeneration zone to regenerate said catalyst.
107. (Originally Presented) The method of Claim 106 wherein the cracking catalyst is fluidized during contacting said hydrocarbon feedstock.
108. (Currently Amended) A fluid cracking catalyst comprising (a) a cracking component suitable for catalyzing the cracking of hydrocarbons and (b) at least 0.1 weight percent of a NO_x reduction zeolite selected from the group consisting ZSM-11, beta, MCM-49, mordenite, MCM-56, Zeolite-L, zeolite Rho, errionite, chabazite, clinoptilolite, MCM-22, MCM-35, MCM-61, Offretite, A, ZSM-12, ZSM-23, ZSM-18, ZSM-22, ZSM-57, ZSM-61, ZK-5, NaJ, Nu-87, Cit-1, SSZ-35, SSZ-48, SSZ-44, SSZ-23, Dachiardite, Merlinoite, Lovdarite, Levyne, Laumontite, Epistilbite, Gmelonite, Gismondine, Cancrinite, Brewsterite, Stilbite, Paulingite, Goosecreekite, Natrolite, omega or mixtures thereof.
109. (Originally Presented) The cracking catalyst of Claim 108 wherein said catalyst comprises integral particles which contain both components (a) and (b).

110. (Originally Presented) The cracking catalyst of Claim 108 wherein component (b) comprises from about 0.1 to about 60 wt % of the cracking catalyst.
111. (Originally Presented) The cracking catalyst of Claim 110 wherein component (b) comprises from about 1 to about 40 wt % of the cracking catalyst.
112. (Originally Presented) The catalyst of Claim 108 further comprising at least one additional NO_x reduction composition.
113. (Originally Presented) The catalyst of Claim 112 wherein the additional NO_x reduction composition is a non-zeolitic composition.
114. (Originally Presented) The catalyst of Claim 113 wherein the additional NO_x reduction composition comprises (a) an acidic metal oxide containing substantially no zeolite; (b) a metal component, measured as the oxide, selected from the group consisting of an alkali metal, an alkaline earth metal and mixtures thereof; (c) an oxygen storage metal oxide component; and (d) at least one noble metal component.
115. (Originally Presented) The catalyst of Claim 112 wherein the additional NO_x reduction composition comprises (a) an acidic metal oxide support; (b) an alkali metal, alkaline earth metal or mixtures thereof; (c) a transition metal oxide having oxygen storage capability; and, (d) a transition metal selected from Groups IB and IIB of the Periodic Table, and mixtures thereof.
116. (Currently Amended) The catalyst of Claim 112 wherein the additional NO_x reduction composition is a low NO_x CO combustion promoter composition which comprises (a) an acidic oxide support; (b) an alkali

metal, an alkaline earth metal or mixtures thereof; (c) a transition metal oxide having oxygen storage capability; and (d) palladium.

117. (Originally Presented) The catalyst of Claim 112 wherein the additional NO_x reduction composition comprises at least one metal-containing spinel which includes a first metal and a second metal having a valence higher than the valence of said first metal, at least one component of a third metal other than said first and second metals and at least one component of a fourth metal other than said first, second and third metals, wherein said third metal is selected from the group consisting of Group IB metals, Group IIB metals, Group VIA metals, the rare-earth metals, the Platinum Group metals and mixtures thereof, and said fourth metal is selected from the group consisting of iron, nickel, titanium, chromium, manganese, cobalt, germanium, tin, bismuth, molybdenum, antimony, vanadium and mixtures thereof.
118. (Originally Presented) The catalyst of Claim 117 wherein the metal containing spinel comprises magnesium as said first metal and aluminum as said second metal.
119. (Originally Presented) The catalyst of Claim 117 wherein the third metal component in the metal containing spinel is selected from the group consisting of a Platinum Group metal, the rare-earth metals and mixtures thereof.
120. (Originally Presented) The catalyst of Claim 117 wherein the third metal component is present in an amount in the range of about 0.001 to about 20 weight percent, calculated as elemental third metal.
121. (Originally Presented) The catalyst of Claim 117 wherein said fourth metal component is present in an amount in the range of about 0.001 to about 10 weight percent, calculated as elemental fourth metal.

122. (Originally Presented) The catalyst of Claim 112 wherein the additional NO_x reduction additive is a zinc based catalyst.
123. (Originally Presented) The catalyst of Claim 112 wherein the additional NO_x reduction additive is an antimony based NO_x reduction additive.
124. (Originally Presented) The catalyst of Claim 112 wherein the additional NO_x reduction additive is a pervoskite-spinel NO_x reduction additive.
125. (Originally Presented) The catalyst of Claim 112 wherein the additional NO_x reduction additive is a hydrotalcite containing composition.
126. (Originally Presented) A method of reducing NO_x emissions from the regeneration zone during fluid catalytic cracking of a hydrocarbon feedstock into lower molecular weight components, said process comprising (a) contacting a hydrocarbon feedstock during a fluid catalytic cracking (FCC) process wherein NO_x emissions are released from a regeneration zone of the FCCU operating under FCC conditions with an FCC cracking catalyst composition of Claim 108; and (b) reducing the amount of NO_x emissions released from the regeneration zone of the FCCU by at least 10 percent as compared to the amount of NO_x emissions released in the absence of the NO_x reduction composition.
127. (Originally Presented) The method of Claim 126 wherein step (b) is accomplished without a substantial change in the hydrocarbon feedstock conversion or yield of cracked hydrocarbons obtained during the FCC process as compared to the hydrocarbon feedstock conversion or yield of cracked hydrocarbons obtained from the cracking catalyst alone.
128. (Originally Presented) The method of Claim 126 or 127 wherein the amount of NO_x reduction zeolite present in the cracking catalyst composition comprises at least about 0.1 wt % of the cracking catalyst composition.

129. (Originally Presented) The method of Claim 126 or 127 wherein the amount of NO_x reduction zeolite present in the cracking catalyst composition ranges from about 0.1 to about 60 wt % of the cracking catalyst composition.
130. (Originally Presented) The method of Claim 129 wherein the amount of NO_x reduction zeolite present in the cracking catalyst composition ranges from about 1 to about 40 wt % of the cracking catalyst composition.
131. (Originally Presented) The method of Claim 126 or 127 wherein the NO_x reduction zeolite is exchanged with a cation selected from the group consisting of hydrogen, ammonium, alkali metal and combinations thereof.
132. (Originally Presented) The method of Claim 126 or 127 wherein the NO_x reduction zeolite further comprises at least one stabilizing metal.
133. (Originally Presented) The method of Claim 132 wherein the stabilizing metal is a metal selected from the group consisting of Groups 2A, 3B, 4B, 5B, 6B, 7B, 8B, 2B, 3A, 4A, 5A the Lanthanide Series of The Periodic Table, Ag and mixtures thereof.
134. (Originally Presented) The method of Claim 133 wherein the stabilizing metal is selected from the group consisting of Groups 3B, 2A, 2B, 3A and the Lanthanide Series of the Periodic Table, and mixtures thereof.
135. (Originally Presented) The method of Claim 134 wherein the stabilizing metal is selected from the group consisting of lanthanum, aluminum, magnesium and zinc, and mixtures thereof.
136. (Originally Presented) The method of Claim 132 wherein the stabilizing metal is incorporated into the pores of the NO_x reduction zeolite.

137. (Originally Presented) The method of Claim 126 or 127 further comprising recovering the cracking catalyst and treating the used catalyst in a regeneration zone to regenerate said catalyst.
138. (Originally Presented) The method of Claim 126 or 127 wherein the cracking catalyst is fluidized during contacting said hydrocarbon feedstock.
139. (Currently Amended) The method of Claim ~~104~~ 105 or 126 further comprising contacting the hydrocarbon feed with at least one additional NO_x reduction additive composition.
140. (Originally Presented) The method of Claim 139 wherein the additional NO_x reduction additive composition is a non-zeolitic composition.
141. (Originally Presented) The method of Claim 140 wherein the additional NO_x reduction additive composition comprises (a) an acidic metal oxide containing substantially no zeolite; (b) a metal component, measured as the oxide, selected from the group consisting of an alkali metal, an alkaline earth metal and mixtures thereof; (c) an oxygen storage metal oxide component; and (d) at least one noble metal component.
142. (Currently Amended) The method of Claim 139 wherein the NO_x reduction additive composition is a low NO_x, CO combustion promoter composition which comprises (a) an acidic oxide support; (b) an alkali metal and/or alkaline earth metal or mixtures thereof; (c) a transition metal oxide having oxygen storage capability; and (d) palladium.
143. (Originally Presented) The method of Claim 139 wherein the additional NO_x reduction additive composition comprises at least one metal-containing spinel which includes a first metal and a second metal having a valence higher than the valence of said first metal, at least one component of a third metal other than said first and second metals and at least one

component of a fourth metal other than said first, second and third metals, wherein said third metal is selected from the group consisting of Group IB metals, Group IIB metals, Group VIA metals, the rare-earth metals, the Platinum Group metals, and mixtures thereof, and said fourth metal is selected from the group consisting of iron, nickel, titanium, chromium, manganese, cobalt, germanium, tin, bismuth, molybdenum, antimony, vanadium and mixtures thereof.

144. (Originally Presented) The method of Claim 143 wherein the metal-containing spinel comprises magnesium as said first metal and aluminum as said second metal.
145. (Originally Presented) The method of Claim 143 wherein the third metal component in the metal-containing spinel is selected from the group consisting of a Platinum Group metal, the rare-earth metals and mixtures thereof.
146. (Originally Presented) The method of Claim 143 wherein the third metal component is present in an amount in the range of about 0.001 to about 20 weight percent, calculated as elemental third metal.
147. (Originally Presented) The method of Claim 143 wherein said fourth metal component is present in an amount in the range of about 0.001 to about 10 weight percent, calculated as elemental fourth metal.
148. (Originally Presented) The method of Claim 139 wherein the additional NO_x reduction additive composition comprises (a) an acidic oxide support; (b) an alkali metal and/or alkaline earth metal or mixtures thereof; (c) a transition metal oxide having oxygen storage capability; and (d) a transition metal selected from the Groups IB and IIB of the Periodic Table.
149. (Originally Presented) The method of Claim 139 wherein the additional NO_x reduction additive composition is a zinc based catalyst.

150. (Originally Presented) The method of Claim 139 wherein the additional NO_x reduction additive composition is an antimony based NO_x reduction additive.
151. (Originally Presented) The method of Claim 139 wherein the additional NO_x reduction additive composition is a pervoskite-spinel NO_x reduction additive.
152. (Originally Presented) The method of Claim 139 wherein the additional NO_x reduction additive composition is a hydrotalcite containing composition.
153. (Originally Presented) The cracking catalyst of Claim 108 wherein component (a) comprises a Y-type zeolite and component (b) is present in an amount sufficient to provide a ratio of NO_x reduction zeolite to Y-type zeolite of less than 2 in the total catalyst.
154. (Originally Presented) The cracking catalyst of Claim 153 wherein component (b) is present in an amount sufficient to provide a ratio of NO_x reduction zeolite to Y-type zeolite of less than 1 in the total catalyst.
155. (Originally Presented) The cracking catalyst of Claim 108 wherein component (b) further comprises at least one stabilizing metal.
156. (Originally Presented) The cracking catalyst of Claim 155 wherein the stabilizing metal is a metal selected from the group consisting of Groups 2A, 3B, 4B, 5B, 6B, 7B, 8B, 2B, 3A, 4A, 5A and the Lanthanide Series of The Periodic Table, Ag and mixtures thereof.
157. (Originally Presented) The cracking catalyst of Claim 156 wherein the stabilizing metal is selected from the group consisting of Groups 3B, 2A,

2B, 3A and the Lanthanide Series of the Periodic Table, and mixtures thereof.

158. (Originally Presented) The cracking catalyst of Claim 157 wherein the stabilizing metal is selected from the group consisting of lanthanum, aluminum, magnesium and zinc, and mixtures thereof.
159. (Originally Presented) The cracking catalyst of Claim 155 wherein the stabilizing metal is incorporated into the pores of component (b).
160. (Originally Presented) The cracking catalyst of Claim 112 wherein the additional NO_x reduction composition comprises (i) an acidic metal oxide, (ii) cerium oxide, (iii) a lanthanide oxide other than ceria, and (iv) optionally, at least one oxide of a transition metal selected from Groups IB and IIB of the Periodic Table, and mixtures thereof.
161. (Currently Amended) The cracking catalyst of Claim ~~163~~ 108 wherein the NO_x reduction zeolite is selected from the group consisting of beta, MCM-49, mordenite, MCM-56, Zeolite-L, zeolite Rho, errionite, chabazite, clinoptilolite, MCM-22, Offretite, A, ZSM-12, ZSM-23, omega and mixtures thereof.
162. (Originally Presented) The cracking catalyst of Claim 108 wherein the NO_x reduction zeolite has a SiO₂ to Al₂O₃ molar ratio of less than 500.
163. (Originally Presented) The cracking catalyst of Claim 108 further comprising a zeolite other than the NO_x reduction zeolite.
164. (Originally Presented) The cracking catalyst of Claim 163 wherein the other zeolite is selected from the group consisting of ferrierite, ZSM-5, ZSM-35 and mixtures thereof.

165. (Originally Presented) The cracking catalyst of Claim 163 or 164 wherein the other zeolite is present in an amount ranging from about 1 to about 80 weight percent of the composition.
166. (Originally Presented) The cracking catalyst of Claim 165 wherein the other zeolite is present in an amount ranging from about 10 to about 70 weight percent of the composition.
167. (Currently Amended) The cracking catalyst of Claim 108 wherein the NO_x reduction zeolite is ~~selected from the group consisting of beta, MCM-49, mordenite, MCM-56, Zeolite L, zeolite Rho, errionite, chabazite, elinoptilolite, MCM-22, Offretite, A, ZSM-12, ZSM-23, omega and mixtures thereof.~~ exchanged with a cation selected from the group consisting of hydrogen, ammonium, alkali metal and combinations thereof.
168. (Originally Presented) The method of Claim 139 wherein the additional NO_x reduction composition comprises (i) an acidic metal oxide, (ii) cerium oxide, (iii) a lanthanide oxide other than ceria, and (iv) optionally, at least one oxide of a transition metal selected from Groups IB and IIB of the Periodic Table, and mixtures thereof.